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1 **Microwave-assisted extraction of sulfated polysaccharides**  
2 **(fucoidan) from brown seaweed**

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26        **ABSTRACT**

27

28        Sulfated polysaccharides (fucoidan) were recovered from brown seaweed *Fucus vesiculosus*  
29        by microwave-assisted extraction (MAE). Different conditions of pressure (30 to 120 psi),  
30        extraction time (1 to 31 min), and alga/water ratio (1/25 to 5/25 g ml<sup>-1</sup>) were evaluated during  
31        this process aiming to establish a condition to maximize the extraction results. The alga  
32        degradation (%), total sugar yield (%), and SO<sub>3</sub> content (%) were also determined to each  
33        experimental condition. All the studied variables presented significant ( $p<0.05$ ) influence on  
34        fucoidan yield. MAE at 120 psi, 1 min, using 1 g alga/25 ml water was the best condition for  
35        the fucoidan recovery. L-fucose was the main constituent of this polysaccharide, which also  
36        contained xylose and galactose. MAE under optimum reaction conditions was an effective  
37        method to recover fucoidan from *Fucus vesiculosus*. This method required short extraction  
38        times, and non corrosive solvents, resulting in reduced costs and being an environmentally  
39        friend technique.

40

41        **Keywords:** Seaweed; *Fucus vesiculosus*; Microwave-assisted extraction; Sulfated  
42        polysaccharides; Fucoidan

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## 51 1. Introduction

52

53 Marine algae, or seaweeds, contain several physiologically bioactive compounds with  
54 important economical relevance, such as polysaccharides and iodine organic products, macro  
55 and micro elements, vitamins and unsaturated fatty acids (Bhakuni & Rawat, 2005; Craigie,  
56 2010). Brown seaweeds are the second most abundant group of marine algae comprising  
57 about 2,000 species. Among them, *Ascophyllum spp.*, *Fucus spp.*, *Laminaria spp.*, *Sargassum*  
58 *spp.*, and *Turbinaria spp.* are the most commonly used on industrial level (Hong, Hien, &  
59 Son, 2007). Recent studies have demonstrated that brown algae contain biologically active  
60 substances that can be used as anticoagulant, antithrombotic, anti-inflammatory, anti-tumor,  
61 contraceptive, and anti-viral, for the treatment of several diseases (Synytsya et al., 2010;  
62 Wang et al., 2010a). Such properties have been attributed to the sulfated polysaccharides  
63 fucoidans in the algae cell wall structure (Ellouali, Boisson-Vidal, Durand, & Jozefonvicz,  
64 1993; Berteau & Mulloy, 2003; Queiroz et al., 2008).

65 Fucoidans may constitute up to 25–30% of the alga dry weight, depending on the  
66 seaweed specie and, to a lesser extent, on season. These polysaccharides are composed by  $\alpha$ -  
67 1,3-backbones or repeating disaccharide units of  $\alpha$ -1,3- and  $\alpha$ -1,4-linked fucose residues with  
68 branchings attached at C2 positions. Depending on the structure of the main chain, fucoidans  
69 may be sulfated at C4, C2 or in both positions of the fucose units. Besides fucose, fucoidans  
70 may also contain mannose, xylose, galactose, and rhamnose sugars, and uronic acids  
71 (Kusaykin et al., 2008; Rodríguez-Jasso, Mussatto, Pastrana, Aguilar, & Teixeira, 2010).

72 Sulfated polysaccharides are generally extractable with hot water, dilute acid, or dilute  
73 alkali, by using large solvents volume and long extraction times (Marais & Joseleau, 2001;  
74 Rioux, Turgeon, & Beaulieu, 2007; Wang, Zhang, Zhang, & Li, 2008; Yang, Chung, & You  
75 2008). In the last decade, microwave-assisted extraction (MAE) has been successfully applied

76 for extraction of numerous biologically active compounds from a wide variety of natural  
77 resources (Sosa-Ferrera, Santana-Rodríguez, & Mahugo-Santana, 2005; Périno-Issartier,  
78 2010; Wang et al., 2010b; Martins, Aguilar, de la Garza-Rodríguez, Mussatto, & Teixeira,  
79 2010). This technique consists in the penetration of microwave energy into the material  
80 structure, which produces a volumetrically distributed heat source due to molecular friction  
81 resulting from dipolar rotation of polar solvents and from the conductive migration of  
82 dissolved ions, accelerating the mass transfer of target compounds. In general, the compounds  
83 are extracted more selectively and quicker by this technique, with similar or better yields in  
84 comparison with conventional extraction processes, using less energy and solvent volume,  
85 thus being more environmentally friend (Eskilsson & Björklund, 2000; Srogi, 2006; Bélanger  
86 & Paré, 2006). Only few works report the use of microwave-based techniques for extraction  
87 of compounds (alkaline galactans, carrageenans, and agar) from seaweeds (Uy, Easteal, Farid,  
88 Keam, & Conner 2005; Navarro, Flores, & Stortz, 2007; Chhatbara, Meena, Prasada, &  
89 Siddhanta, 2009; Sousa, Alves, Morais, Delerue-Matos, & Gonçalves, 2010).

90 The present study evaluated the extraction of sulfated polysaccharides (fucoidan) from  
91 *Fucus vesiculosus* seaweed by MAE technique. An experimental design was applied to verify  
92 the influence of pressure, extraction time and alga/water ratio in the response of fucoidan  
93 yield, and the condition able to maximize the extraction yield was established. The percentage  
94 of alga degradation, total sugar yield in the hydrolysates after MAE, and SO<sub>3</sub> content were  
95 also determined to each experimental condition. Characterization of the recovered fucoidan  
96 was performed by HPLC, FTIR, and TGA/DSC analyses.

97

## 98 **2. Material and methods**

99

### 100 *2.1. Chemicals*

101

102 Anthrone reagent was purchased from Prolabo, Normapur, Merck; 3,5-dinitrosalicylic  
103 acid from Fluka, Chemika, and Coomassie Plus (Bradford) assay kit was from Thermo  
104 Scientific Co. Other reagents were all of analytical grade.

105

## 106 2.2. *Alga collection and sample preparation*

107

108 *Fucus vesiculosus* seaweed was collected from the Praia Norte, Viana do Castelo,  
109 Portugal, during September 2009. After collected the algal material was washed with fresh  
110 water in order to remove salt, sand and epiphytes, dried at 35 °C, and milled using a home  
111 blender. Particles lower than 1000 µm were not used in experiments. Milled material was kept  
112 in plastic bags at room temperature for use in the extraction experiments. Material samples  
113 were analyzed to determine the moisture and ash contents (AOAC official methods). The total  
114 sugars content present in the alga composition was determined after sulfuric acid hydrolysis  
115 for 2 h under vigorous agitation.

116

## 117 2.3. *Extraction procedure*

118

119 MAE experiments were performed in a digestion oven model MDS-2000 (CEM  
120 Corporation, Matthews, NC). For each experiment, reaction vessels interconnected with  
121 tubing were placed in the sample holder, a rotating carousel. One of the vessels was equipped  
122 with pressure sensor that measured and controlled the set point within the cell.

123 For the extraction reactions, milled seaweed was suspended in the desired amount of distilled  
124 water and placed into the extraction vessel. The suspensions were irradiated under different  
125 pressures, for times varying between 1 and 31 minutes. Conditions of alga/water ratio,

126 pressure and time used in each experiment are shown in Table 1. After irradiation, the vessels  
 127 were immediately cooled in ice bath and the suspensions were filtrated through nylon fiber to  
 128 separate the residual alga, which was dried at 35 °C, weighted to determine the residual  
 129 amount obtained (value that was also used to calculate the alga degradation, % AD), and  
 130 stored. An aliquot of each obtained hydrolysate was taken for total sugar quantification (%  
 131 TS- $A_{MAE}$ ). Subsequently, 1% (w/v) CaCl<sub>2</sub> solution was added to the liquid fraction and the  
 132 mixture was maintained overnight at 4 °C for alginate removal. The fraction obtained by  
 133 ionization of CaCl<sub>2</sub> was separated by filtration. Double volume of ethanol absolute was added  
 134 to the resultant filtrate and the mixture was stored at 4 °C for 8 h. Ethanol-precipitated  
 135 polysaccharide was recovered by centrifugation (8,500 rpm, 15 min, 4 °C), dried at 35 °C,  
 136 milled and stored for further analyses. Fucoidan extraction yield (% Fuc), alga degradation (%  
 137 AD), and total sugar yield of hydrolysates after microwave-assisted extraction (% TS- $A_{MAE}$ ),  
 138 were calculated according to Eq.1-3, where  $WM_{OH}$  is the dry mass weight obtained after  
 139 ethanol precipitation;  $WA$  is the alga weight used in each experiment;  $WA_{MAE}$  is the dry alga  
 140 weight recovered after MAE;  $TS_{H_{MAE}}$  is the mg of total sugars in the hydrolysates obtained  
 141 after MAE; and  $TS_A$  is the mg of total sugars in the alga *Fucus vesiculosus* (35.12 mg  
 142 TS/100 mg alga).

$$143 \quad \%Fuc = \frac{WM_{OH}}{WA} \times 100 \quad (1)$$

$$144 \quad \%AD = \left( \frac{WA - WA_{MAE}}{WA} \right) \times 100 \quad (2)$$

$$145 \quad \%TS - A_{MAE} = \left( \frac{TS_{H_{MAE}}}{TS_A} \right) \times 100 \quad (3)$$

146

#### 147 2.4. Characterization of the recovered fucoidan

148

149 A mass of 10-15 mg of the recovered fucoidan was submitted to hydrolysis with 4 N  
150 HCl (2 ml) at 121 °C for 2 h. After the hydrolysis reaction, the total sugar content in the liquid  
151 fraction was determined by the anthrone method (using glucose as standard), and the content  
152 of sulfate groups was determined by turbidity through the barium chloride–gelatin method  
153 (Dodgson, 1961). All absorbance measurements were performed in triplicate.

154 For the determination of monosaccharides content by HPLC, 10-15 mg of the recovered  
155 fucoidan was hydrolyzed with 2 M trifluoroacetic acid (0.5 ml) at 121 °C for 2 h, in glass  
156 tubes sealed with N<sub>2</sub>. After reaction, the tubes were cooled in ice-water bath, centrifuged  
157 (5000 rpm, 5 min), and the liquid fraction was neutralized to pH 7 with 2 M NaOH. Resulting  
158 samples were then injected into the HPLC system. A Jasco chromatograph system equipped  
159 with a refraction-index detector and a MetaCarb 87P (300 × 7.8 mm) column at 80 °C was  
160 used for the sugars determination. Deionized water was used as mobile phase at a flow rate of  
161 0.4 ml min<sup>-1</sup>.

162 Micrographs of seaweed samples before and after extraction were obtained by scanning  
163 electron microscopy using a Nova NanoSEM 200 microscope. For the analyses, the samples  
164 were fixed on a specimen holder with aluminum tape and then sputtered with gold in a  
165 sputter-coater under high vacuum condition. Images were obtained at magnification of 2000  
166 fold.

167 Thermal gravimetric analysis (TGA) data were taken with a thermo balance model  
168 TGA-50 (Shimadzu Corporation, Kyoto, Japan) in a nitrogen atmosphere. Differential  
169 scanning calorimetry (DSC) analyses were performed using a Modulate DSC-50 (Shimadzu  
170 Corporation, Kyoto, Japan). Mass samples of 10-13 mg were run from room temperature to  
171 600 °C, at a rate of 10 °C min<sup>-1</sup>.

172 Infrared analysis spectroscopy (FTIR) was carried out on a Perkin-Elmer 16 PC  
173 spectrometer (Boston, USA) using 16 scans and frequency range of 400-4000 cm<sup>-1</sup>. For FT-IR



174 measurement, the polysaccharide was ground with spectroscopic grade potassium bromide  
 175 (KBr) powder and then pressed into 1 mm pellets. The vibration transition frequencies of each  
 176 spectrum were baseline corrected and the absorbance was normalized between 0 and 1.

177

### 178 2.5. Experimental design

179

180 A  $2^3$  full experimental design with four replicates at the centre point was used to  
 181 evaluate the effects of the variables pressure ( $X_1$ ; psi), time ( $X_2$ ; min), and alga/water ratio ( $X_3$ ;  
 182 g ml<sup>-1</sup>) on the extraction of fucoidan under MAE conditions. For statistical analysis, the  
 183 variables were coded according to Eq. 4, where each independent variable is represented by  $x_i$   
 184 (coded value),  $X_i$  (real value),  $X_0$  (real value at the centre point), and  $\Delta X_i$  (step change value).  
 185 The real and coded values of the variables are given in Table 1. Low and high factors were  
 186 coded as -1 and +1; the centre point was coded as 0.

$$187 \quad x_i = (X_i - X_0) / \Delta X_i \quad (4)$$

188 Four assays at the centre point of the design were carried out to estimate the random  
 189 error needed for the analysis of variance, as well as to examine the presence of curvature in  
 190 the response surfaces. The fucoidan yield ( $Y_1$ ; % Fuc), alga degradation ( $Y_2$ ; % AD), total  
 191 sugar yield of hydrolysates after MAE ( $Y_3$ ; % TS- $A_{MAE}$ ), and the sulfate content ( $Y_4$ ; % SO<sub>3</sub>)  
 192 were taken as dependent variables or responses of the experimental design. The results were  
 193 analyzed by analysis of variance (ANOVA), and the responses and variables (in coded unit)  
 194 were correlated by response surface analysis to obtain the coefficients of Eq. 5.

$$195 \quad Y_i = a_0 + a_1x_1 + a_2x_2 + a_3x_3 + a_{12}x_1x_2 + a_{13}x_1x_3 + a_{23}x_2x_3 \quad (5)$$

196 In Eq. 5,  $Y_i$  represents the response or dependent variable;  $a_0$  is the interception  
 197 coefficient;  $x_1$ ,  $x_2$  and  $x_3$  are the coded levels of the three variables (pressure, time and alga  
 198 mass/water volume ratio), and  $a_1$ ,  $a_2$ ,  $a_3$ ,  $a_{12}$ ,  $a_{13}$ ,  $a_{23}$  are the regression coefficients. The

199 statistical significance of the regression coefficients was determined by Student's *t*-test, and  
200 the proportion of variance explained by the models was given by the multiple coefficient of  
201 determination,  $R^2$ . Statistica 5.0 was the software used for data analysis.

202

### 203 **3. Results and discussion**

204

#### 205 *3.1. Alga characterization*

206

207 *Fucus vesiculosus* contained a moisture content of  $15.95 \pm 0.08\%$  (w/w). This value is  
208 higher than those reported to other marine algae such as *Laminaria* (6.64%) and *Gigartina*  
209 (9.86%) (Gómez-Ordóñez, Jiménez-Escrig, & Rupérez, 2010), and is a positive aspect  
210 considering the alga use in MAE because the moisture content is closely related to the  
211 absorption efficiency of microwaves by the immersed target material. The water molecules  
212 convert the microwave energy into heat, resulting in a sudden rise of the temperature inside  
213 the material. The temperature keeps rising until the internal pressure exceeds the capacity of  
214 expansion of the matrix thus creating an explosion at the intermolecular level. As a  
215 consequence, the substances that are located within these chemical systems migrate to the  
216 surrounding medium that traps and dissolves them (Bélanger & Paré, 2006).

217

218 Ashes in *Fucus vesiculosus* corresponded to  $18.32 \pm 0.83\%$  (w/w), a high value  
219 currently found in seaweeds, but much higher than those generally observed in terrestrial  
220 vegetables. Ashes content comprises the minerals present in the material. Although the  
221 minerals present in *Fucus vesiculosus* ashes were not determined here, brown seaweeds have  
222 been reported to have high chloride content, small amounts of fluoride, nitrate and phosphate,  
223 and trace amounts of nitrite and bromide. Due to the significant mineral content present in  
their chemical composition, several seaweeds have been used as food supplement to help

224 meet the recommended daily intakes of some minerals and trace elements (Gómez-Ordóñez et  
225 al., 2010)

226 Total sugars content in *Fucus vesiculosus* was  $35.12 \pm 0.02\%$  (w/w). This value is lower  
227 than those reported by Rioux et al. (2007) for brown seaweeds, and probably, it is a  
228 consequence of the period in which the alga was harvested. Algae generate their biomass  
229 reserve after the rapid grow phase in spring in order to survive the winter where hardly any  
230 photosynthesis occurs. As a consequence, a larger amount of polysaccharides is found during  
231 the winter season. In the present study, the alga was harvested in September (autumn season),  
232 which was not the best collection period.

233

### 234 3.2. Operational variables affecting fucoidan extraction by MAE

235

236 Several studies report MAE as a technique able to produce biopolymers with high molar  
237 mass at significantly shorter heating times than conventional extraction methods (Chen, Liu,  
238 Jiang, & Zeng, 2005; Leonelli & Mason, 2010). Considering this aspect and the structural and  
239 chemical complexity of sulfated polysaccharides, MAE was used in the present study to  
240 extract fucoidan from algal material. It was also expected that by using this method fucoidan  
241 would undergo degradation. In this work the microwave energy over the target material was  
242 controlled under pressure parameter, because one of the most frequent problems of heating by  
243 microwave fields is the temperature measurements, which are complicated by the presence of  
244 high intensity electromagnetic fields (Kustov & Sinev, 2010).

245 The used extraction conditions, including pressure, extraction time and algae/water ratio  
246 were selected based on previous studies for the production of other heteropolymers by MAE,  
247 such as pectin from citric peels or sugar beet pulp (Fishman, Chau, Hoagland, & Ayyad,  
248 2000; Fishman, Chau, Cooke, & Hotchkiss, 2008). Pressure conditions, particularly, were

249 evaluated until the maximal operational value allowed by the equipment. Fig. 1 shows the  
250 pressure profiles against heating time of microwave irradiation for a sample load of 1 g per 25  
251 ml of water. Heat stages rates were estimated measuring the ramp up and ramp down through  
252 the heating and cooling phases between the isothermal periods of the extraction procedures.  
253 The equivalent temperature used to each pressure (after the system has reached a saturated  
254 vapor behavior) was estimated using tables of water liquid-vapor phase and corresponded to  
255 122, 152 and 172 °C for 30, 75, and 120 psi, respectively. As can be seen in Fig. 1, the  
256 samples reached the hydrothermal stage (constant pressure) in less than 2 min, showing  
257 similar pressure increment with heating rates of around 103-128 °C min<sup>-1</sup>. On the contrary,  
258 the pressure reduction showed that cooling rates were dependent of the quantity of time that  
259 the sample was irradiated at the isothermal stage. As a consequence, the compounds  
260 hydrolysis is also influenced at the cooling phase.

261 Moreover, the time required to attain the desired pressure was also dependent of the  
262 number of vessels processed simultaneously in the equipment, and therefore, the number of  
263 vessels should be chosen in order to minimize the time needed to reach the set conditions and  
264 to avoid a “bumping” phenomenon during the extraction (Eskilsson & Björklund, 2000).  
265 The solid/liquid ratio, i.e., the ratio between alga mass and water volume used for the  
266 reactions, is also an important parameter to be considered in MAE. The product recovery by  
267 conventional extraction methods is usually increased when using high solvent volumes  
268 (Eskilsson & Björklund, 2000); however, similar behavior may not occur in MAE. For this  
269 reason, different solid/liquid ratios varying from 1/25 to 5/25 g ml<sup>-1</sup> were evaluated in the  
270 present study. Table 1 shows the conditions of pressure, reaction time and alga/water ratio  
271 used in each experimental MAE assay, and the respective fucoidan yield, alga degradation,  
272 total sugar yield and sulfate content obtained. Great variation in all the responses was

273 observed according to the used experimental condition. Fucoidan yield, for example, was  
274 increased in up to 17 times, by varying the MAE conditions.

275 All the studied operational variables affected the extraction process, presenting  
276 significant main effects and/or interactions for all of the evaluated responses (Table 2). For  
277 fucoidan yield, the alga/water ratio presented a significant main effect ( $p<0.05$ ) of negative  
278 signal, which reveals that the fucoidan yield was increased when using an alga/water ratio of  
279 1 g/25 ml. Although the pressure and extraction time have not shown significant main effects  
280 for fucoidan yield, interaction between these variables was highly significant ( $p<0.01$ ) for this  
281 response. When observing the main effects of these two variables for the other responses, it  
282 can be observed that pressure had a significant main effect of positive signal for all of them,  
283 which suggests that the extraction results were improved when the pressure was increased. As  
284 a consequence, since the interaction between pressure and reaction time had a significant  
285 negative effect for fucoidan yield response, it can be concluded that the use of lower reaction  
286 times favored the extraction process. This analysis is in agreement with the results presented  
287 in Table 1, which shows that the highest fucoidan yield (18.22%) was obtained when the  
288 highest pressure (120 psi) and the lowest extraction time (1 min) and alga/water ratio (1 g/25  
289 ml) were used (conditions of the assay 5).

290 Similar behavior was reported by (Latha, 2007) during the biopolymers extraction by  
291 MAE. According to this author, the particle concentration increase promotes a strong  
292 absorption of the microwave energy near the surface of the vessel, and low penetration depth  
293 of microwave radiation, which reduces the percentage of extraction. On the other hand, the  
294 pressure increase promotes the temperature raise in a direct proportion. As a consequence, the  
295 extraction rate increases due to the viscosity and surface tension reduction (Eskilsson &  
296 Björklund, 2000).

297 In the present study, despite the pressure increase has favored the fucoidan yield,  
 298 equipment limitations did not allow to evaluate pressure values higher than 120 psi.  
 299 Additionally, the use of alga/water ratios lower than 1/25 g ml<sup>-1</sup> might not be economically  
 300 advantageous for the process since it would increase the costs for fucoidan recovery from the  
 301 liquid phase. Therefore, the optimal MAE conditions for fucoidan extraction from *Fucus*  
 302 *vesiculosus* were established in the studied range of operational values. An analysis of  
 303 variance of the obtained data for linear models gave high values for the coefficient of  
 304 determination R<sup>2</sup> (between 0.84 and 0.95), which show a close agreement between  
 305 experimental results and the theoretical values predicted by the first-order polynomials. A  
 306 multiple regression analysis was then performed to fit first-order polynomial equations to the  
 307 experimental data points. The fucoidan yield (Y<sub>1</sub>, %), alga degradation (Y<sub>2</sub>, %), total sugar  
 308 yield of hydrolysate (Y<sub>3</sub>, %), and the sulfate content (Y<sub>4</sub>, %) were correlated as a function of  
 309 extraction pressure (x<sub>1</sub>), time (x<sub>2</sub>) and alga/water ratio (x<sub>3</sub>) (coded values) used for MAE,  
 310 resulting in Eqs. 6, 7, 8, and 9, respectively.

$$311$$

$$312 \quad Y_1 = 10.30 + 1.29x_1 + 0.05x_2 - 2.58x_3 - 4.17x_1x_2 + 0.46x_1x_3 + 0.53x_2x_3 \quad (R^2 = 0.84) \quad (6)$$

$$313 \quad Y_2 = 46.19 + 7.50x_1 + 5.96x_2 - 4.72x_3 - 2.74x_1x_2 - 2.89x_1x_3 - 3.24x_2x_3 \quad (R^2 = 0.92) \quad (7)$$

$$314 \quad Y_3 = 11.64 + 2.79x_1 + 1.81x_2 - 9.26x_3 - 2.51x_1x_2 - 2.02x_1x_3 - 1.44x_2x_3 \quad (R^2 = 0.95) \quad (8)$$

$$315 \quad Y_4 = 24.34 + 3.06x_1 + 4.17x_2 + 1.37x_3 + 0.81x_1x_2 + 0.92x_1x_3 + 1.19x_2x_3 \quad (R^2 = 0.94) \quad (9)$$

316

317 Three-dimensional response surfaces described by the above-mentioned first-order  
 318 polynomials were well fitted to the experimental data points through flat surfaces, confirming  
 319 the suitability of the proposed linear models to explain the responses variations in the studied  
 320 range of values. Fig. 2 represents the variations in fucoidan yield according to the pressure  
 321 and alga/water ratio used for extraction. As can be seen, the flat surface clearly indicates a

322 region where the value of this response is maximized, which corresponds to the use of 120  
323 psi, and 1/25 alga/water ratio ( $\text{g ml}^{-1}$ ) during 1 min of extraction. The highest fucoidan  
324 extraction yield (18.22% in a dry weight basis) is in good agreement with the values reported  
325 by Rioux et al. (2007) during the extraction of *F. vesiculosus* by 3 sequential hydrolysis steps  
326 (each one of 3 h) at 70 °C. Moreover, this value was higher than those reported for fucoidan  
327 obtained from other sources extracted by hydrothermal conventional procedures under  
328 temperatures between 25 and 70 °C and times of 2-6 h (Zvyagintseva et al. 1999; Duarte,  
329 Cardoso, Nosedá, & Cerezo, 2001; Navarro, D. A., Flores, M. L., & Stortz, C. A., 2007).  
330 Additionally, Yang et al. (2008) evaluated the hydrolysis of sulfated polysaccharides of *U.*  
331 *pinnatifida* testing twice microwave for 30-120 sec and founded that microwave heating  
332 around 30-60 seconds only was more effective in improving the polymer dissolution.

333 Fig. 3 shows the alga structure before and after MAE under optimum conditions. As can  
334 be seen, the untreated sample (Fig. 3A) presented closed cells and rough surfaces, which were  
335 mostly destroyed after MAE (Fig. 3B). A less destructive effect of destruction in the alga  
336 structure was observed after MAE under milder pressure conditions (Fig. 3C). Such facts  
337 evidence the importance of the pressure increase on the extraction process, as commented  
338 before. The alga structure after MAE under high pressure (120 psi, Fig. 3B) was formed by a  
339 very rough surface with many cavities, suggesting that microwave radiation had the power on  
340 cuticular layer destruction, as observed also by other authors (Chen et al., 2005).

341

### 342 3.3. Characterization of the extracted fucoidans

343

#### 344 3.3.1. Compositional analysis

345 The fucoidans obtained in all the experimental MAE conditions were characterized  
346 regarding the monosaccharide and sulfate contents (Table 3). L-Fucose was the only

347 monosaccharide found in all the samples. Galactose was also present in most of the samples,  
348 but xylose was only present in some of them. The results presented in Table 3 suggest that the  
349 pressure used for extraction had a strong influence on the fucoidan composition, since the  
350 galactose contents in the fucoidan structure were increased when the pressure used for  
351 extraction was increased to 120 psi; and only fucose was present in the fucoidans obtained at  
352 30 psi. Similarly, xylose was only present in structures obtained at 120 psi. Under the  
353 optimum MAE conditions, a fucoidan structure composed predominantly by fucose, followed  
354 by significant proportion of xylose and minor galactose content was obtained (Table 3, assay  
355 5). This is in agreement with literature data that report that fucoidan from *F. vesiculosus* has a  
356 heterogeneous and branched structure (Marais & Joseleau, 2001).

357 Besides the monosaccharide content, the conditions used for MAE affected also the  
358 fucoidans sulfating degree (Table 3). However, high sulfate content (> 20%) was found in  
359 practically all the fucoidan samples, which is an advantageous aspect since sulfate groups  
360 have been reported to have important biological functions such as anti-HIV activity; and such  
361 activity is potentially increased when the sulfating degree is increased (Schaeffer & Krylov,  
362 2000). Additionally, the presence of non-sulfate monosaccharide units in polysaccharides  
363 branches is reported to annul the anticoagulant effect of the polysaccharide (Costa et al.,  
364 2010). The ratio between total sugars and sulfate content (TS/SO<sub>3</sub>, Table 3) is considered an  
365 indicator of the anticoagulant activity of fucoidan polysaccharides (Wang et al., 2008). In the  
366 present study, most of the experiments showed TS concentrations similar or higher than SO<sub>3</sub>  
367 concentrations.

368 Fucoidan polymers from other sources had comparable amounts of sulfates (19–30%)  
369 and monosaccharide composition with fucose as the major sugar in the extracted fucoidans  
370 (50-90 % mol) and lower amounts of galactose and xylose (Zvyagintseva et al. 1999; Duarte  
371 et al. 2001; Rioux et al. 2007). However, it is important emphasizing that chemical



372 composition of fucoidan polymers is significantly dependent on species, anatomical regions,  
373 growing conditions, extraction procedures and analytical methods.

374

### 375 3.3.2. *Thermal analysis*

376 TGA and DSC curves of fucoidan extracted under optimum MAE conditions are  
377 showed in Fig. 4. Three different stages were well defined during these analyses. The first one  
378 was basically associated with the weight loss (moisture) due to dehydration, which covered a  
379 temperature range between 25 °C and 110 °C. Subsequently, pyrolysis reactions of the sample  
380 started at 120 °C. The second stage started at 195 °C and consisted in the devolatilization of  
381 the sample, with evolution of the volatile matter mainly occurring between 220 °C and 490  
382 °C. Finally, the third stage began close to 500 °C and was maintained up to 600 °C. The  
383 remaining mass at the end of this process (around 50% of the original fucoidan mass)  
384 corresponds to the ash content in the sample. This residual mass is probably constituted by  
385 sulfates, phosphates and carbonates, which are minerals usually found in polysaccharides  
386 structures like fucoidan (Anastasakis, Ross, & Jones, 2011).

387

### 388 3.3.3. *FTIR analysis*

389 Fucoidan obtained under optimum MAE conditions, as well as fucoidan samples  
390 obtained under other evaluated extraction conditions, were analyzed by FTIR to determine  
391 the specific absorption bands present in the recovered products. The FTIR spectra in Fig. 5  
392 clearly show that all the evaluated samples exhibited absorption bands typical of fucoidans.  
393 The absorption band at 1240–1255  $\text{cm}^{-1}$  (S=O stretching) confirmed the presence of sulfate  
394 in the recovered polysaccharides. The sharp band at 840  $\text{cm}^{-1}$  and the shoulder at 820  $\text{cm}^{-1}$   
395 (C-S-O) suggest a complex pattern of substitution, primarily at C-4 position (axial C-4

396 substitution of  $\alpha$ -linked L-fucopyranose) with other substitution at C-2 or/and C-3 (equatorial  
397 positions) in lower amount (Marais & Joseleau, 2001; Wang et al., 2010a)

398

#### 399 **4. Conclusions**

400

401 In summary, MAE under optimum reaction conditions was an effective method to  
402 recover fucoidan from *Fucus vesiculosus*. This method required short extraction time and use  
403 of non corrosive solvents, resulting in reduced costs when compared to the conventional  
404 extraction techniques. Additionally, MAE can be considered a more environmentally friend  
405 technique than the traditional extraction processes, since it requires lower energy  
406 consumption and generates less wastes. For all these reasons, MAE was considered a  
407 potential method to obtain fucoidan from brown seaweed.

408

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410

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417

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542 **Figure captions**

543

544 **Fig. 1.** Pressure profiles as a function of radiation time during MAE of *Fucus vesiculosus* for  
545 fucoidan recovery; relation between heating and cooling rates ( $^{\circ}\text{C}/\text{min}$ ). Sample load: 1 g  
546 alga/ 25 ml water. A) 30 psi (122  $^{\circ}\text{C}$ ) / 1min; B) 30 psi (122  $^{\circ}\text{C}$ ) / 31min; C) 75 psi (152  $^{\circ}\text{C}$ ) /  
547 16min; D) 120 psi (172  $^{\circ}\text{C}$ ) / 1min; and E) 120 psi (172  $^{\circ}\text{C}$ ) / 31min.  $\Delta\text{H}$ : heat rate (1);  $\Delta\text{C}$ :  
548 cool rate (2).

549

550 **Fig. 2.** Response surface fitted to the experimental data points corresponding to the fucoidan  
551 yield during MAE of *Fucus vesiculosus*.

552

553 **Fig. 3.** Scanning electron micrographs of *Fucus vesiculosus*: (A) untreated sample; (B)  
554 sample obtained after MAE at 120 psi, 1 min, using 1 g alga/ 25 ml water; (C) sample  
555 obtained after MAE at 30 psi, 31 min, using 1 g alga/ 25 ml water. Magnification: 2000-fold.

556

557 **Fig. 4.** TGA and DSC thermograms of fucoidan sample obtained under optimum MAE  
558 conditions.

559

560 **Fig. 5.** Infrared analysis spectroscopy (FTIR) of fucoidan samples obtained by MAE of  
561 *Fucus vesiculosus* under different operational conditions.

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567 **Highlights**

568

569 Fucoidan was recovered from brown seaweed by microwave-assisted extraction.

570 Pressure, extraction time, and alga/water ratio affected the fucoidan yield.

571 Extraction conditions able to maximize the fucoidan recovery were established.

572 Recovered fucoidan was constituted by fucose, xylose and galactose.

573 MAE with short extraction time was effective to recover fucoidan from seaweed.

574

575

576

577

**Table 1**

Experimental conditions used for MAE of *Fucus vesiculosus* according to a  $2^3$  full experimental design. Real and (coded) values of the operational variables pressure ( $x_1$ ), extraction time ( $x_2$ ) and alga/water ratio ( $x_3$ ), and results obtained for the responses fucoidan yield ( $Y_1$ ; % Fuc), alga degradation ( $Y_2$ ; % AD), total sugar yield of hydrolysates after MAE ( $Y_3$ ; % TS- $A_{MAE}$ ), and sulfate content ( $Y_4$ ; %  $SO_3$ ).

Assay	Variables <sup>a</sup>						Responses			
	$x_1$		$x_2$		$x_3$		$Y_1$ (% Fuc)	$Y_2$ (% AD)	$Y_3$ (% TS- $A_{MAE}$ ) <sup>b</sup>	$Y_4$ (% $SO_3$ )
1	30	(-1)	1	(-1)	1/25	(-1)	6.25	28.82	9.42	20.08
2	30	(-1)	1	(-1)	5/25	(+1)	1.08	27.92	1.39	16.87
3	30	(-1)	31	(+1)	1/25	(-1)	15.61	48.99	24.52	22.76
4	30	(-1)	31	(+1)	5/25	(+1)	8.60	42.57	3.59	27.63
5	120	(+1)	1	(-1)	1/25	(-1)	18.22	51.36	27.62	21.09
6	120	(+1)	1	(-1)	5/25	(+1)	10.93	46.33	4.39	24.88
7	120	(+1)	31	(+1)	1/25	(-1)	6.93	67.98	25.54	30.31
8	120	(+1)	31	(+1)	5/25	(+1)	5.74	42.59	3.68	35.55
9	75	(0)	16	(0)	3/25	(0)	12.53	48.76	9.65	23.07
10	75	(0)	16	(0)	3/25	(0)	13.24	50.51	10.01	22.57
11	75	(0)	16	(0)	3/25	(0)	12.16	47.02	8.56	24.99
12	75	(0)	16	(0)	3/25	(0)	12.36	51.40	11.36	22.33

<sup>a</sup> pressure ( $x_1$ ): psi; time ( $x_2$ ): min; alga/water ratio ( $x_3$ ): g ml<sup>-1</sup>. <sup>b</sup> % TS- $A_{MAE}$  was calculated by the ratio between mg of total sugars in the hydrolysates obtained after MAE, and mg of total sugars in the alga (35.12 mg/100 mg).

**Table 2**

Effect estimates (EE), standard errors (SE) and level of significance ( $p$ ) for fucoidan yield ( $Y_1$ ; % Fuc), alga degradation ( $Y_2$ ; % AD), total sugar yield of hydrolysates after MAE ( $Y_3$ ; % TS- $A_{MAE}$ ), and sulfate content ( $Y_4$ ; %  $SO_3$ ) obtained after MAE of *Fucus vesiculosus* according to a  $2^3$  full experimental design.

Variables	$Y_1$ (% Fuc)		$Y_2$ (% AD)		$Y_3$ (% TS- $A_{MAE}$ ) <sup>a</sup>		$Y_4$ (% $SO_3$ )	
	EE $\pm$ SE	$p$	EE $\pm$ SE	$p$	EE $\pm$ SE	$p$	EE $\pm$ SE	$p$
$x_1$	2.57 $\pm$ 1.99	0.2521	14.99 $\pm$ 3.19	0.0053 ***	5.58 $\pm$ 2.19	0.0512 *	6.12 $\pm$ 1.31	0.0055 ***
$x_2$	0.10 $\pm$ 1.99	0.9618	11.93 $\pm$ 3.19	0.0134 **	3.63 $\pm$ 2.19	0.1580	8.33 $\pm$ 1.31	0.0014 ***
$x_3$	-5.17 $\pm$ 1.99	0.0482 **	-9.44 $\pm$ 3.19	0.0315 **	-18.51 $\pm$ 2.19	0.0004 ***	2.67 $\pm$ 1.31	0.0970
$x_1x_2$	-8.34 $\pm$ 1.99	0.0085 ***	-5.49 $\pm$ 3.19	0.1460	-5.02 $\pm$ 2.19	0.0700 *	1.61 $\pm$ 1.31	0.2733
$x_1x_3$	0.93 $\pm$ 1.99	0.6609	-5.78 $\pm$ 3.19	0.1298	-4.03 $\pm$ 2.19	0.1245	1.84 $\pm$ 1.31	0.2188
$x_2x_3$	1.07 $\pm$ 1.99	0.6147	-6.47 $\pm$ 3.19	0.9816	-2.88 $\pm$ 2.19	0.2446	2.38 $\pm$ 1.31	0.1288

Significance level: 99% (\*\*\*); 95% (\*\*); 90% (\*).  $x_1$ : pressure (psi);  $x_2$ : time (min);  $x_3$ : alga/water ratio ( $g\ ml^{-1}$ ).

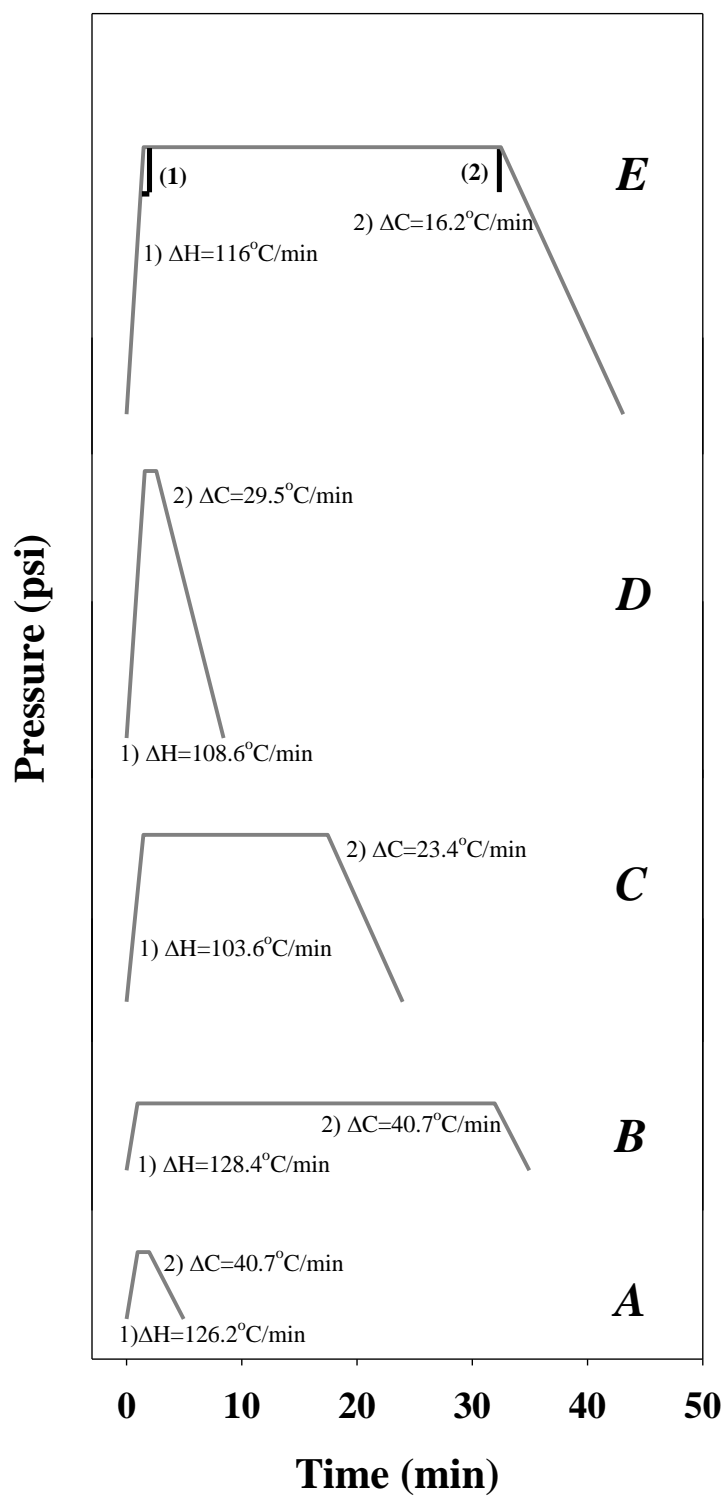
<sup>a</sup> % TS- $A_{MAE}$  was calculated by the ratio between mg of total sugars in the hydrolysates obtained after MAE, and mg of total sugars in the alga (35.12 mg/100 mg).

**Table 3**

Monosaccharide and sulfate composition of fucoidan isolated from *Fucus vesiculosus* by MAE under different operational conditions according to a 2<sup>3</sup> full experimental design. Monosaccharide amount are expressed as the percent of the total sugar content in the sample, in moles.

Assay	Pressure (psi)	Extraction time (min)	Alga/water ratio (g ml <sup>-1</sup> )	Fucose (% mol)	Galactose (% mol)	Xylose (% mol)	TS/SO <sub>3</sub> *
1	30	1	1/25	100.0	0.0	0.0	1/1.00
2	30	1	5/25	100.0	0.0	0.0	1/0.89
3	30	31	1/25	100.0	0.0	0.0	1/0.89
4	30	31	5/25	82.3	17.6	0.0	1/1.07
5	120	1	1/25	53.8	10.8	35.3	1/0.77
6	120	1	5/25	57.4	42.5	0.0	1/0.96
7	120	31	1/25	27.1	42.9	29.9	1/1.84
8	120	31	5/25	39.1	60.8	0.0	1/2.11
9	75	16	3/25	49.0	50.9	0.0	1/1.12
10	75	16	3/25	49.8	50.1	0.0	1/0.93
11	75	16	3/25	53.6	46.3	0.0	1/0.96
12	75	16	3/25	57.6	42.3	0.0	1/1.02

\* TS/SO<sub>3</sub> = (mg TS/100 mg fucoidan)/(mg SO<sub>3</sub>/100 mg fucoidan). TS: total sugars.

**Fig. 1.**

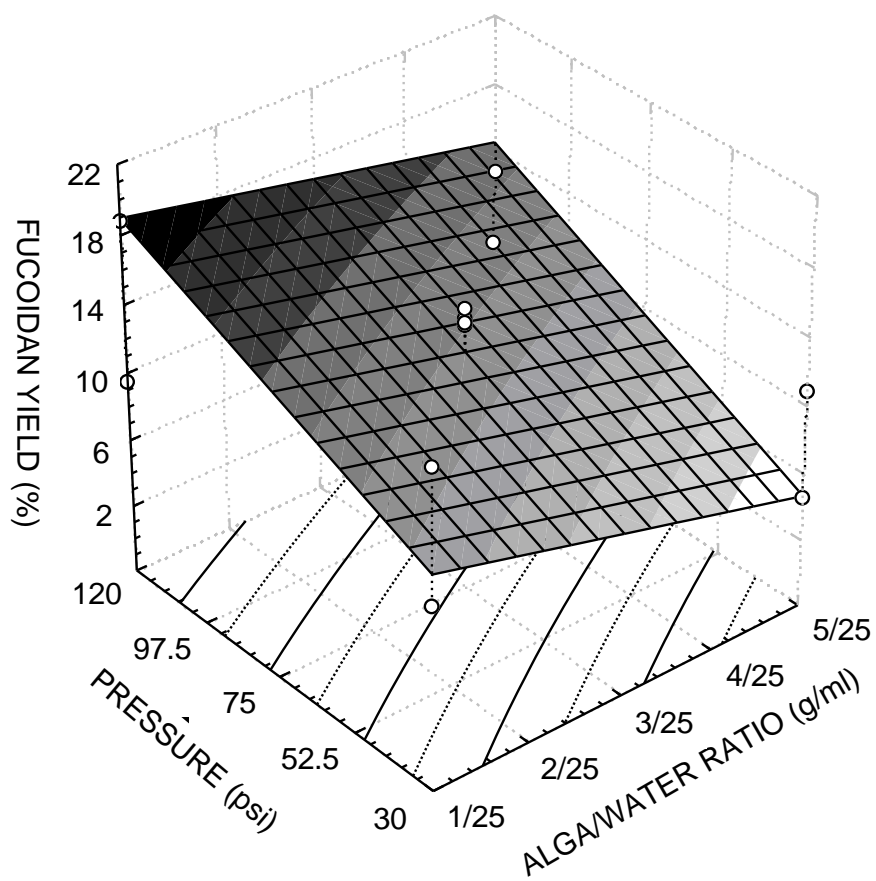


Fig. 2.

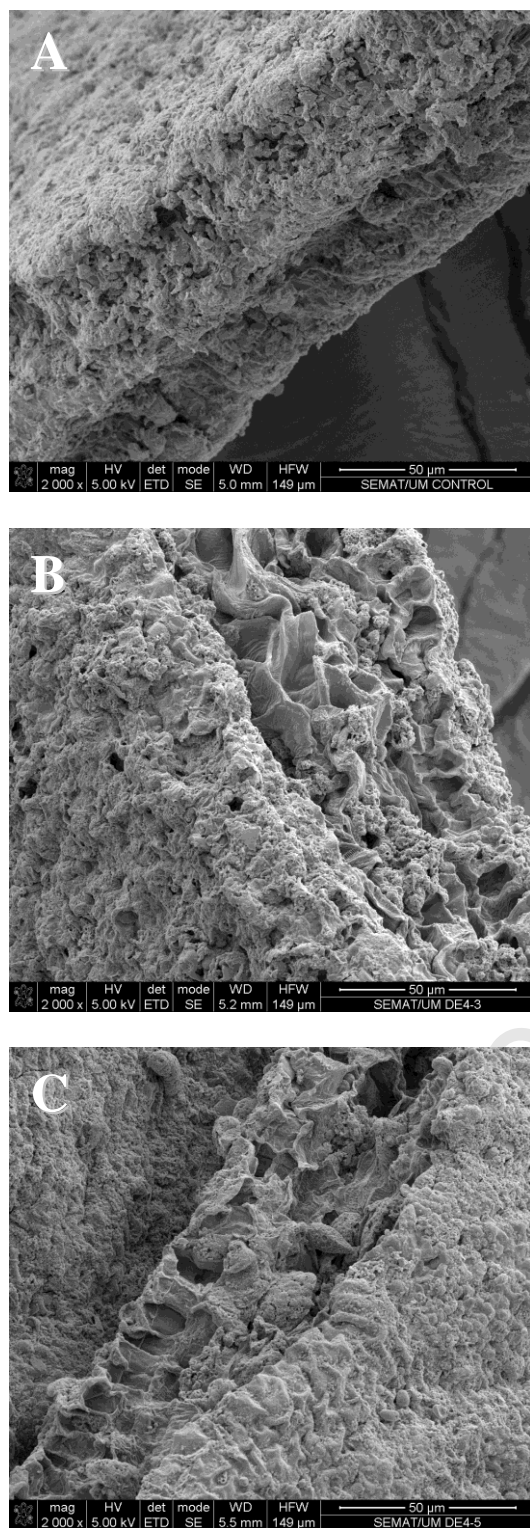


Fig. 3.

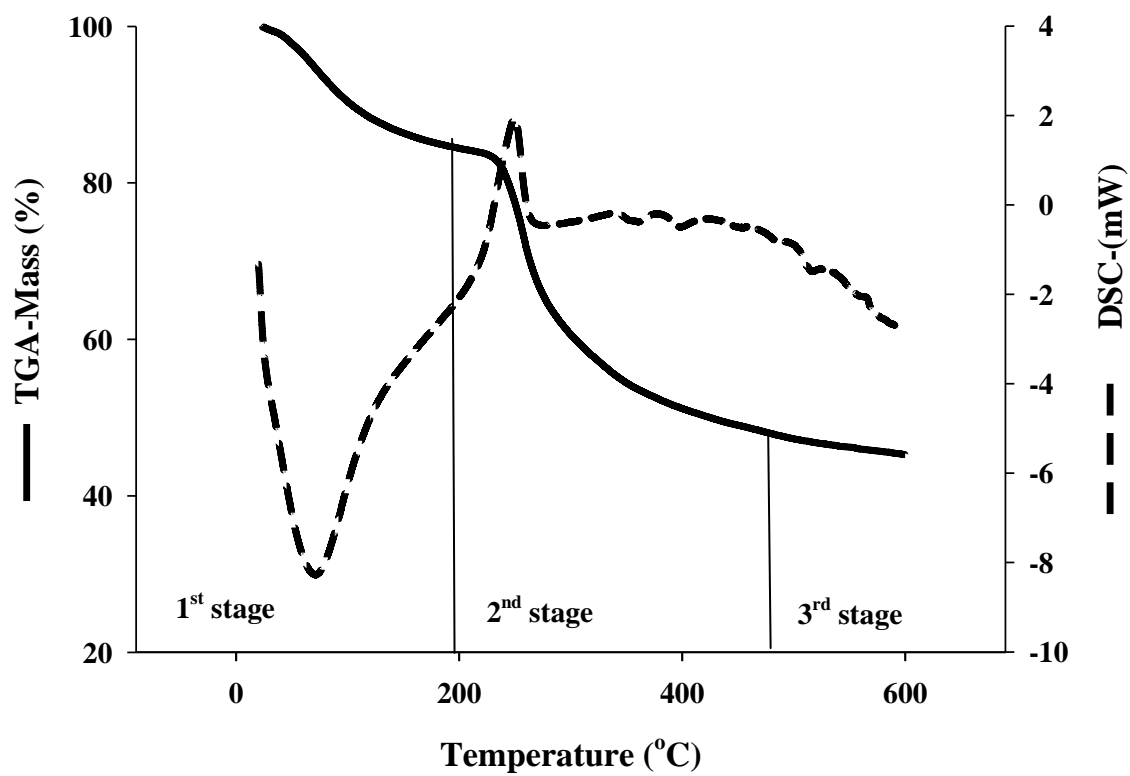


Fig. 4.



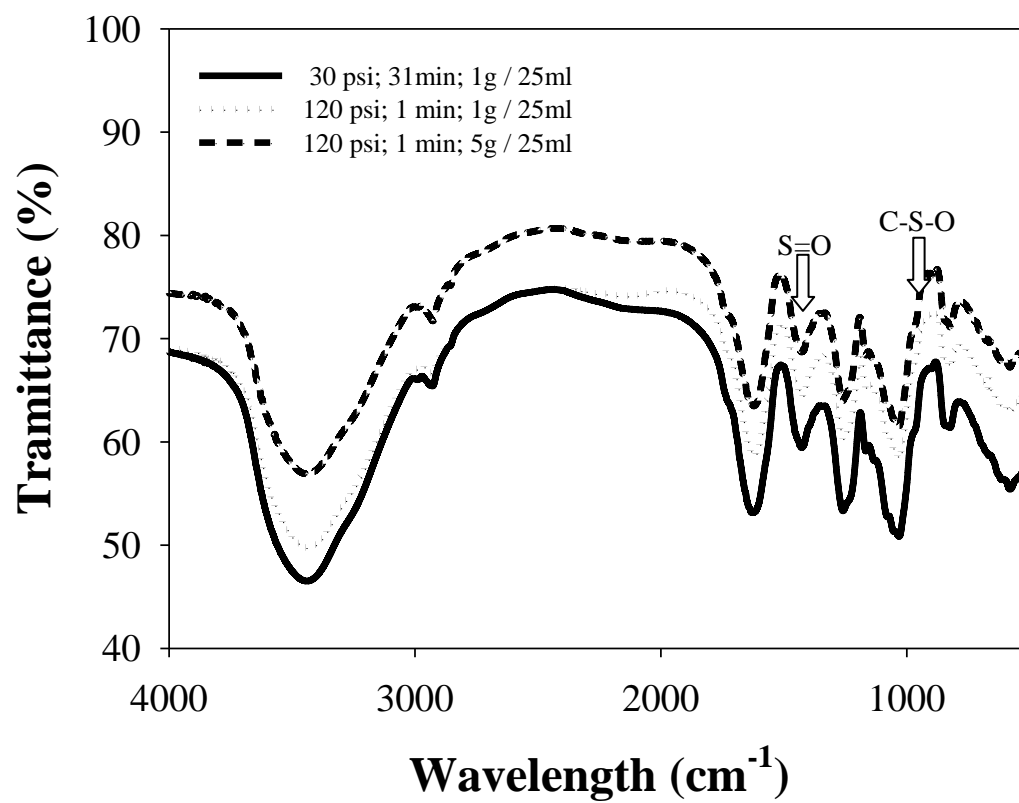


Fig. 5.