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#### New insights on boiling carbon dioxide flow in mini- and micro-channels for optimal silicon detector cooling

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New insights on boiling carbon dioxide flow in mini- and microchannels for optimal silicon detector cooling

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# Introduction

- Along with the general mass and volume minimization, the thermal management needs of future silicon detectors are steadily increasing
- This requires highly effective active cooling in very small channels
- CO<sub>2</sub> in boiling state has been adopted as preferred refrigerant

# **Studied Parameters**

The test range for the two different detector cooling approaches is for

#### **Tubular evaporators:**

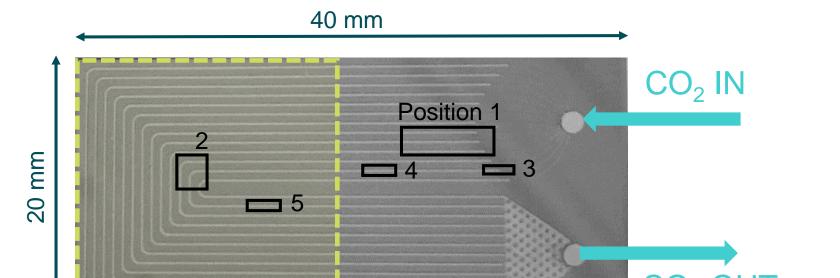
• saturation temperatures (T<sub>sat</sub>) from +15 to -25°C, mass fluxes from 1200 to 100 kg/m<sup>2</sup>s and heat fluxes from 5 to 35 kW/m<sup>2</sup>

#### **Multi-micro-channels:**

• saturation temperatures from +15 to -25°C, mass flow rates of 0.1 g/s and 0.3

# **Visual Results**

## **EXAMPLE : multi-micro-channels**



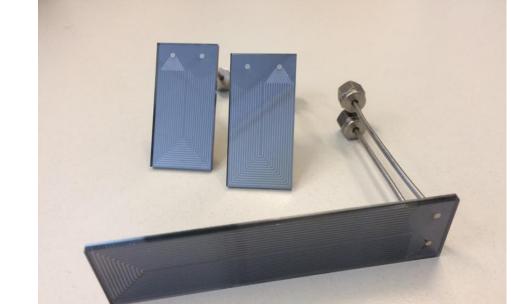
- for the future generations of silicon detectors at the LHC
- However, available data on CO<sub>2</sub> boiling in small channels is too limited – made difficult by the high pressure of  $CO_2$  and often affected by too large measurement uncertainties - to allow for developing reliable predictive models
- To confront these shortcomings a long-term experimental study has been launched with the ambitious objective of developing a deeper understanding of the properties of boiling flows of  $CO_2$  in small channels

# **Experimental Approach**

## The properties of evaporative $CO_2$ are studied within:

- simple small-diameter **tubular evaporators** (stainless steel, L = 0.2 m)
- complex multi-microchannel cooling devices (silicon-substrate bonded to 2 glass for visualization purposes)





g/s and surface power densities from 1 to 5 W/cm<sup>2</sup>

Following parameters are studied with an unprecedented level of accuracy (experimental uncertainty below 10 %  $\leftrightarrow$  typically ~ 20 %)

Tubular evaporators	Multi-micro-channels	
Heat Transfer Coefficient <i>h</i> Pressure drop Δ <i>h</i> top-bottom along the tube	<ul> <li>Thermal Figure of Merit</li> <li>Pressure drop</li> <li>Bubble dynamics in the channels</li> </ul>	
Combination of results leads to new insights on CO <sub>2</sub> poiling in small channels and its dependency on T <sub>sat</sub>		
Parametrical Results		
AMPLE Tubular evaporators		

1 mm inner diameter (ID) stainless steel tube, L = 0.2 m

	CO <sub>2</sub> OUT
2 x 2 cm <sup>2</sup> metallized silicon heate simulating a chip footprint (e.g. Al M. Garcia-Sciveres, et al., The FE-I4 pixel readout	<b>0</b>
	um x 120 µm, length ~ 55 – 80 mm
High speed camera recordings we	ere carried out at the shown
positions along the channels for d for 3 W/cm <sup>2</sup> and 0.3 g/s	ifferent T <sub>sat</sub> and examples are given
<b>Position 1</b> : 13600 fps	
	15 °C : bubble size is in the order of microns or less
	5 °C : bubble size is in the order of a few tens of microns or less
	-25 °C : bubble size is in the order of the channel size
Position 2 : 100000 fps	T <sub>sat</sub> ↓ : general
15 °C: uninterrupted flow o	hubble size ^
5 °C: flow of bubbles with intermittent vapour slugs	
-25 °C: vapour slugs and lic	quid film along walls predominant



## ~ 20 mm

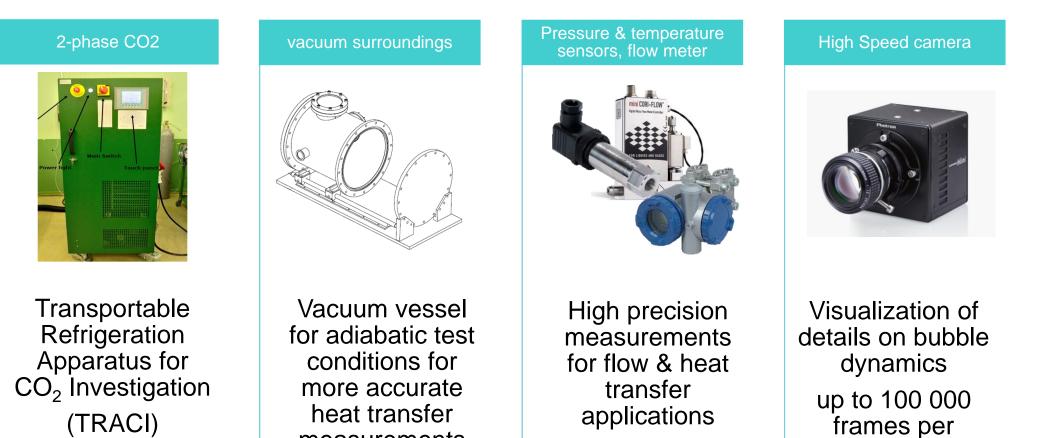
Fig. 1 tubular evaporators

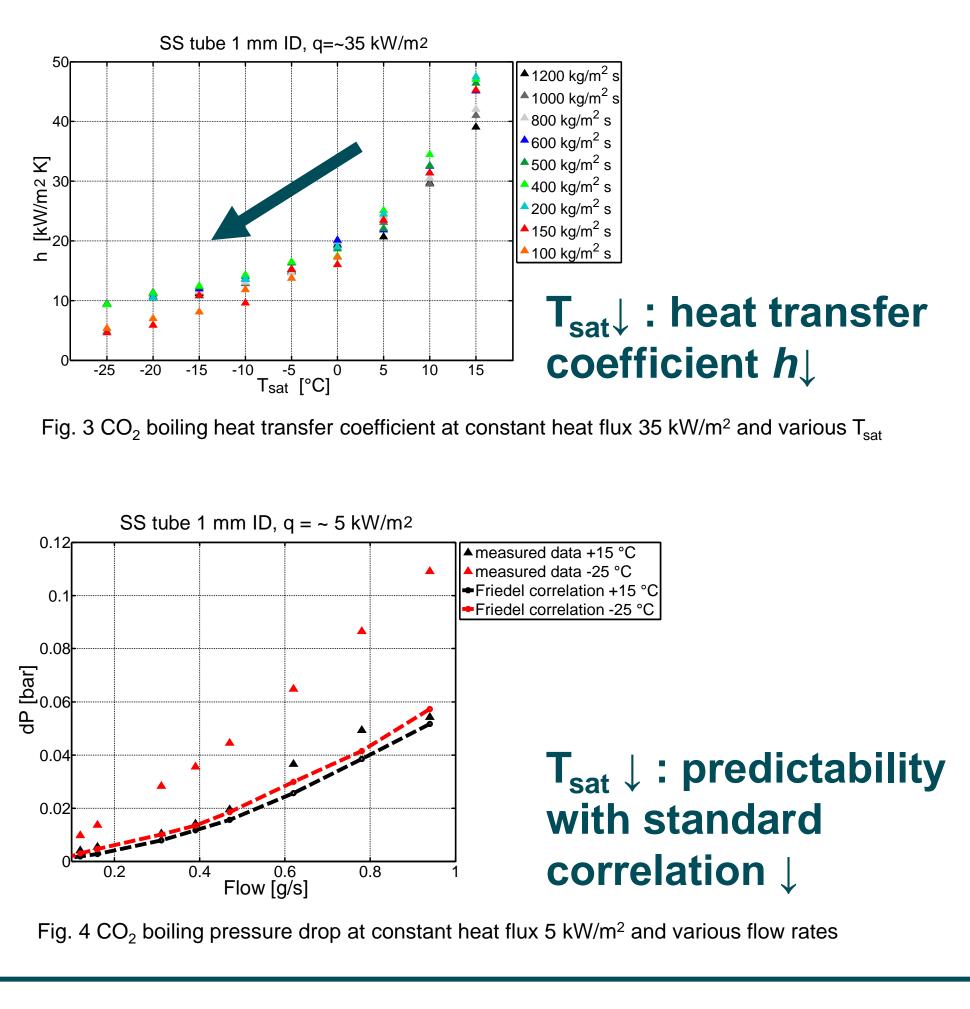
#### Fig. 2 silicon-embedded multi-micro-channels

- Both applications are **highly relevant for HEP experiments**
- Results from the more basic single-channels can complement the rather multifaceted findings from the multi-micro-channels and vice versa
- Thus it is possible to address the need of a deeper understanding of CO<sub>2</sub> boiling properties at mini- and micro-scales at all temperatures of interest on various levels

# **Experimental Setup**

A very versatile new test setup was built with following main components:

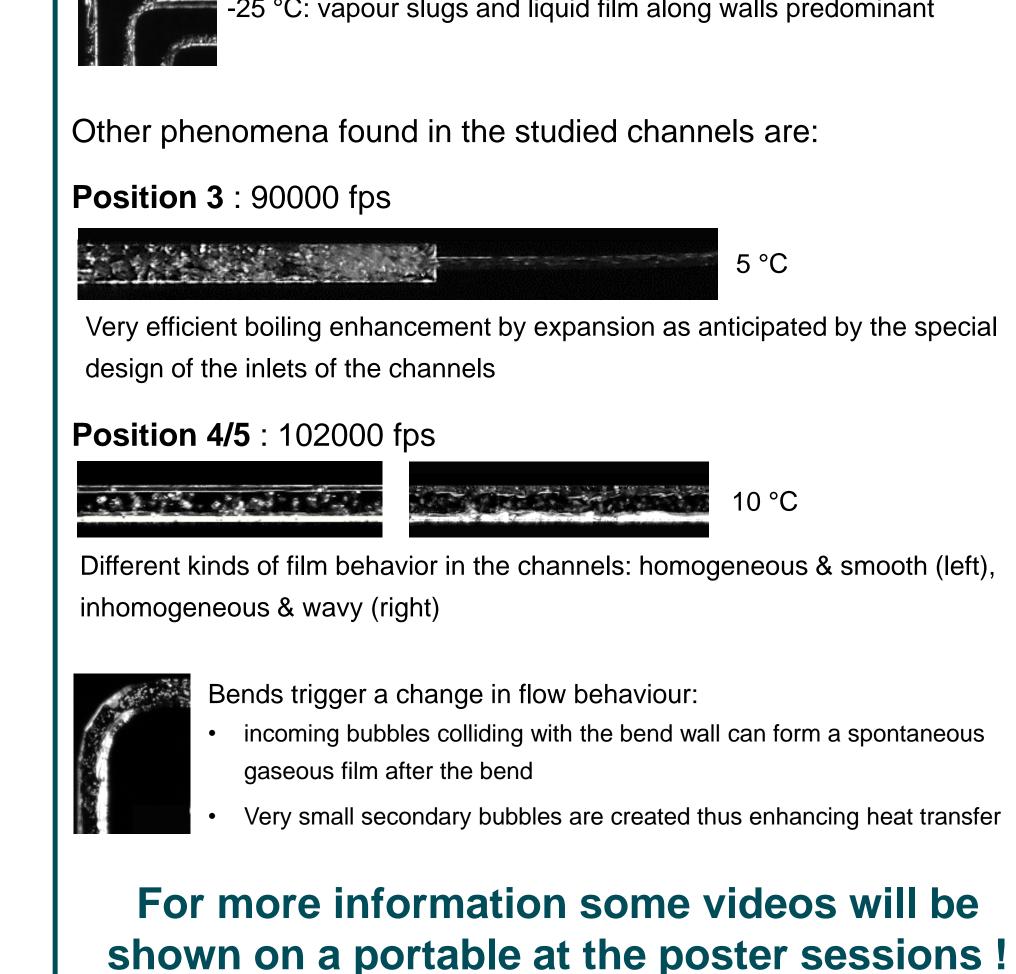




## **EXAMPLE : multi-micro-channels**

200 µm x 120 µm channels in silicon-substrate bonded to glass

multi-micro-channels, g=~3 W/cm<sup>2</sup>

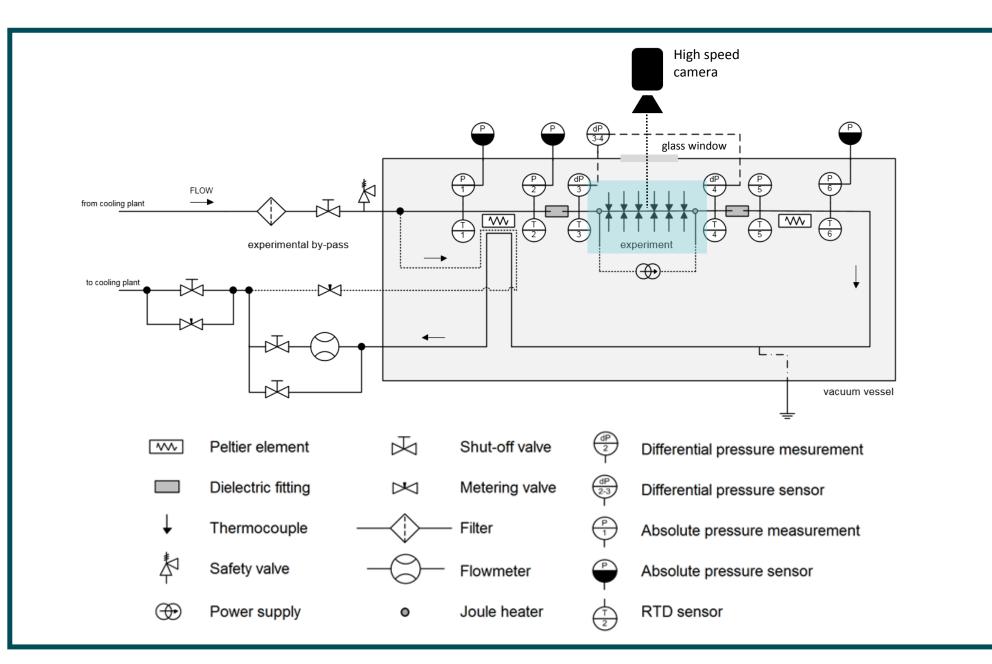


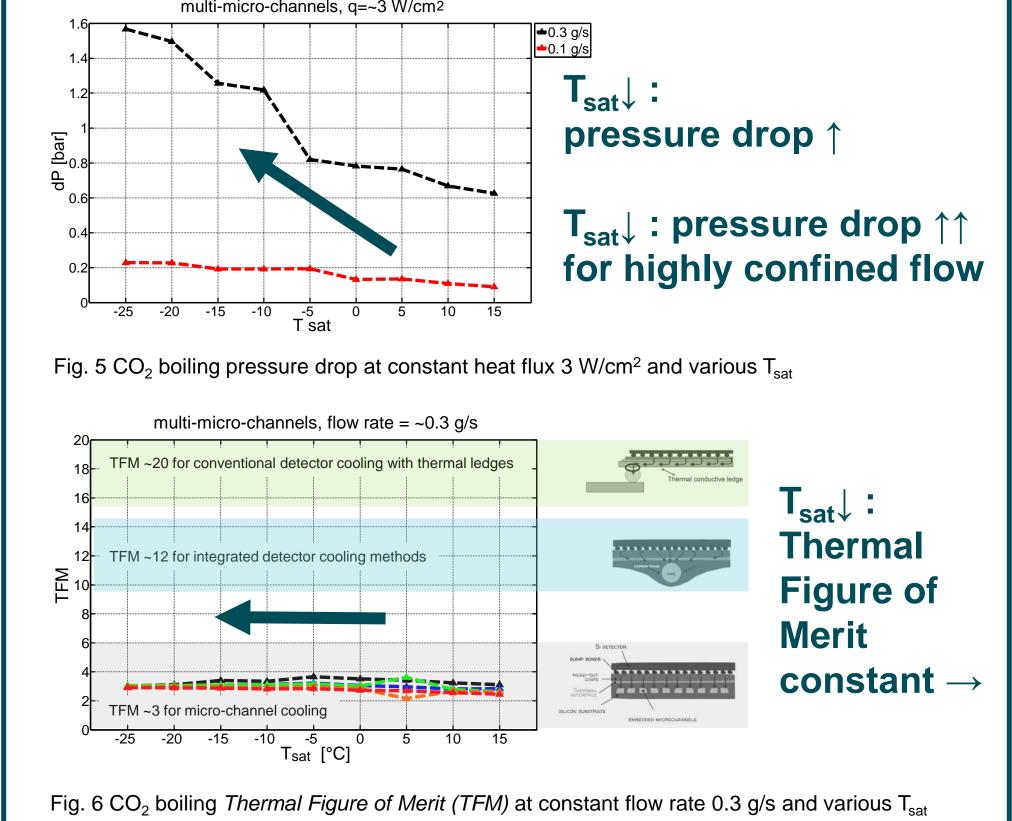
# **Combined Conclusion**

• In general investigations with changing T<sub>sat</sub> and heat flux showed shifting trends of the heat transfer coefficient h, suggesting a shift of the dominating boiling mechanism from high  $T_{sat}$  to low  $T_{sat}$ 



The schematic layout of the test stand is shown below with the interchangeable experimental section at its core:





Different boiling mechanisms are due to **different bubble** dynamics in the channels which can cause different pressure drop and heat transfer coefficient results

- The Thermal Figure of Merit of the tested micro-channels is ~3 for the entire test range, which is a factor 4 better than the best performing conventional detector cooling method
- The qualitative observations from the high-speed visualizations on micro-channels provide a consistent key of interpretation of the quantitative measurements

The examples show that T<sub>sat</sub> greatly affects the boiling properties of CO<sub>2</sub> in small channels and that new advanced models based on this new findings can enhance the design optimization of future mini- and micro-channel evaporators

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